

# FLAMELESS PRESSURIZED OXY-COAL

## Sulcis Technology Center FPOC 50 MWth Large Pilot

a step-ahead in technology development  
of a ready-for-CCS competitive and retrofittable  
carbon-capture solution

# agenda

- FPOC at Sulcis “Clean Energy” Technology Centre
- FPOC performance validation at 50 MWth
- Review of FPOC competitive positioning  
vs CCS competitors  
FPOC «ready for CCS» vs SCPC
- Scale up philosophy and analysis

A CONSORTIUM BETWEEN SOTACARBO AND ENEA

is managing

THE CONSTITUTION of a CENTER OF EXCELLENCE for CLEAN ENERGY TECHNOLOGY

based on

PRESSURIZED OXY-COMBUSTION TECHNOLOGY

contributed by

ITEA Spa (Sofinter Group)

It will materialize the more promising R&D Project for Coal CCS Technology

that ITALY contributes to Environment SAVING

## CCS FLAMELESS PRESSURIZED OXY-COMBUSTION R&D PROJECTS AND RELEVANT GRANTS

2014    2015    2016    2017    2018    2019    2020    2021    2022    2023



Centre of  
Excell. on **8.4 M€**  
Clean Energy



Sulcis Pilot (50 MW<sub>th</sub>)  
pressurized oxyfuel **30 M€**



Demonstration (350 MW<sub>e</sub>)  
pressurized oxyfuel

**1200 M€**

(1)

Italian law 21 Feb. 2014, N. 9:

Incentive for covering CCS extra costs: 30 €/MWh; maximum: 2.100 GWh/yr.

**(1) 60 M€/y = 1.2 Billion € in 20 years**

# Why Flameless Pressurized Oxy-Coal Combustion FPOC

## FPOC: Process Validation

- ❑ 5 MW<sub>th</sub> oxy pilot station has been erected ten years ago by ITEA in cooperation with ENEA
- ❑ Extended validation tests done (ITEA – ENEL – ENEA – Sotacarbo) - Key results analysis with M.I.T. support

Blower

Boiler

Reactor



Fumes:  
Water  
Condensation

Fumes  
Neutralization

Feeding  
set

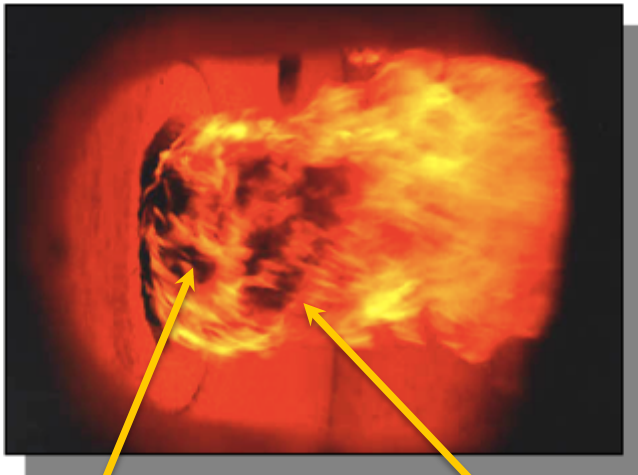
## FPOC

### FPOC: Picturing Innovative Process Fundamentals

Traditional “flame” combustion

“chaotic”

non locally controllable



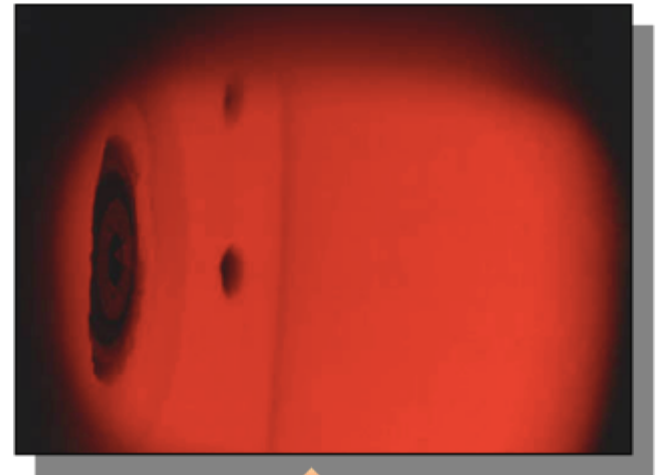
Cool Zone

Flame Front:  
Peak Temperatures

Itea «Flameless combustion »

*MILD, flameless, « volume combustion »*

volume expanded - controllable



High Uniform Temperature

# FPOC

## FPOC: Innovative Approach to Combustion

### TRADITIONAL APPROACH TO COMBUSTION

#### Flame combustion

- Chaotic process/non controllable
- Formation of dangerous products during combustion
- Expensive/complex fumes treatment lines
- Heavy and Fly ashes with questionable disposal
- Plants with limited rangeability
- Low CO<sub>2</sub> concentration in outlet fumes



### NEW APPROACH

#### Flameless oxy-combustion

- High and uniform temperature
- Total absence of dangerous products during combustion
- Simple fumes treatment
- Incombustible ashes reduced to vitrified inert slugs
- High plant rangeability (10 => 100%) at constant performance
- High CO<sub>2</sub> concentration in outlet fumes
- Flexible fuel

## FPOC

### FPOC: A new way of burning at “near zero” emission

- ❑ The lowest emissions rank that known combustion technologies can guarantee.
- ❑ The ashes are reduced to totally inert vitrified beads.
- ❑ 95-98% of introduced heat (LHV) is recovered.
- ❑ High rangeability of the combustion process (from 10% to 100% at constant emission performance)
- ❑ Extended acceptance of water content in the fuel (LHV as low as 4-5 MJ/kg)
- ❑ Ease in commercial CO<sub>2</sub> recovery for different utilizations
- ❑ Capability to simultaneously burn different kinds of waste and fuels
- ❑ Compact relatively small plant, highly automated
- ❑ Competitive CAPEX.



## FPOC

### Established Performances - on the basis of the experience already done

- ❑ Few unit operations; fumes «as such» recycled to combustor and hot fumes quencher
- ❑ Flexible Fuel : quality and low rank coal with almost the same efficiency and emission
- ❑ Coal can be fed as grinded (not pulverized ) slurry with water: slurry logistic avoids coal dust pollution
- ❑ Coal ashes are disposed as vitrified zero-Carbon inert pearls; therefore can be used as recycled material
- ❑ A plant based on this technology can easily follow daily cycling requirements of the grid
- ❑ “Clean” fumes produced allows power recovery from hot fumes turboexpansion
- ❑ “Clean” fumes, concentrated CO<sub>2</sub> (>90%) ease a simple, inexpensive, CO<sub>2</sub> caption process (compression an condensation only)

## FPOC: Competitive Positioning

### Background for Economics Comparison

This technology (in CCS and “ready for CCS set up) is subject to comparison with both:

- ❑ competing CCS technologies
- ❑ current state of art of SC coal fired power plants (in non-CCS set up)

Considering:

- ❑ 550 MWe net Super Critical coal power station baseline
- ❑ Figures relevant to overall hardware installed
- ❑ Standard methods (DOE-NETL) – LCOE
- ❑ Key indexes: CAPEX (Capital Expenditure), LCOE (Levelized Cost of Energy)

- We intend as «ready for CCS» a coal power plant, based on flameless oxy-combustion, that produces fumes, ultra low emission level, constituted by concentrated CO<sub>2</sub> delivered to the atmosphere
- Such plant can be retrofitted with modular units for compression and storage of CO<sub>2</sub>, in accordance with the entity of CO<sub>2</sub> permitted emissions
- With a retrofitting corresponding to the complete transformation to a 100% CCS coal power plant, the final LCOE cost should remain in the range of 20% cost increase for standard quality coal and 10% cost increase for low quality coal.
- The LCOE of such a plant corresponding to the LCOE presented before with cost deduction of the non compressed and stored CO<sub>2</sub> portion

# FPOC

## CCS Technologies Competitive Positioning; Base Line: SC Power Station

| Parameter                                | unit    | Non-CCS      | CCS          |                |                          |   |  | CCS ready          |
|--|---------|--------------|--------------|----------------|--------------------------|---|--|--------------------|
|  |         |              | Post capture | Oxy-combustion |                          |   |  |                    |
|  |         | SC base line | SC + amine   | IGCC (1)       | Atmospheric Oxy-Comb (1) | FPOC Flameless Pressurized Oxy-comb (1) | FPOC optimized (post 50 MWt pilot) (1) | FPOC CCS ready (1) |
| Power in                                 | MWth    | 1345         | 1880         | 1770           | 1760                     | 1520                                    | 1425                                   | 1425               |
| Gross Power                              | MWe     | 580          | 661          |                | 786                      | 723                                     | 681                                    | 681                |
| Net Power                                | MWe     | 550          | 550          | 550            | 550                      | 550                                     | 550                                    | 613                |
| Efficiency                               | %       | 40.9         | 29.3         | 31.0           | 31.3                     | 36.2                                    | 38.6                                   | 42.9               |
| Capital                                  | M€      | 936          | 1693         | 2403           | 2350                     | 1690                                    | 1390                                   | 1210               |
| CAPEX                                    | €/kWnet | 1700         | 3078         | 4370           | 4270                     | 3700                                    | 2710                                   | 1974               |
| LCOE                                     | €/MWh   | 76           | 133          | 140            | 137                      | 104                                     | 91                                     | 75                 |
| LCOE with low rank coal (-35% coal cost) |         |              |              |                |                          | 94 (2)                                  | 82 (2)                                 | 68 (2)             |

Note: Location in Europe - Quality coal - CO2 storage not included

Elaborated according to std methods (DOE-NETL)

(1) Recent advance 0.16 kWh/kg O2 applied to all Oxy-combustion technologies

(2) FPOC only performs low rank coals, with efficiency and Opex almost equivalent to quality coals

## FPOC

### FPOC Industrial Development Pathway

#### 50 MWt large pilot unit at Sulcis

Highlights on key improvements to be validated at Sulcis pilot

- ❑ Efficiency improvement (LHV basis) from 36,2 % to 38,6 %
- ❑ CAPEX reduction from 3700 to 2710 €/KWe net
- ❑ Levelized Cost Of Energy, CCS set up, from 104 to 91 €/MWh (with quality coal)

and  
the dominant technology development problem

Validation of Combustor Scale up Rules

to make future Demo and Industrial Unit bankable

## FPOC: Combustor Scale-Up

### Mandatory Combustor Scale-up Objectives

- ❑ Maintain emission performance, with the same volumetric efficiency
- ❑ Combustor rangeability (5% standby to 100% load) at constant emission performance
- ❑ Rapid (< 30' from standby) load uptake and downs
- ❑ Firing block without any draw back on hardware

## FPOC: Combustor Scale-Up

FPOC theoretically allows different combustor set-up.



Selection of the more promising combustor set up

based on process fundamentals analysis

- ❑ To maintain the best “isothermal” (flat temperature) profile
- ❑ To maintain the fastest feeding heat up speed
- ❑ To reduce molten slag steady hold up
  
- ❑ To avoid wall temperature decline in heat demanding combustor zone, nearby feeding and fumes recycle inlet (to avoid slag viscosity increase and thickening)

## FPOC: Combustor Scale-Up

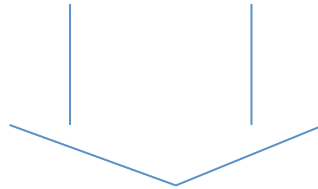
Process analysis concluded:

established once-through, horizontal set up:

- could be limited in scale, with low LHV (low rank) fuels
- lower performer vs scale up objectives

while, vertical, in-and-out (feeding, exiting fumes) from the top set up:

- fulfils (best fit) with all scale up objectives
- towards combustor of 500+ MWt module and above



Vertical set up became the choice for next technology development step



## FPOC: Combustor Scale-Up

### Vertical Set up

#### ACTIONS IN PROGRESS

- Sulcis 50 MWt large pilot have been consequentially engineered.
- Physical-chemical, fluid-dynamics, numerical model elaboration is in progress.
- Erection of a vertical scaled down (5 MWt) combustor is in progress  
(completion and commissioning October 2015) at ITEA 5 MWt pilot unit

to finally perform

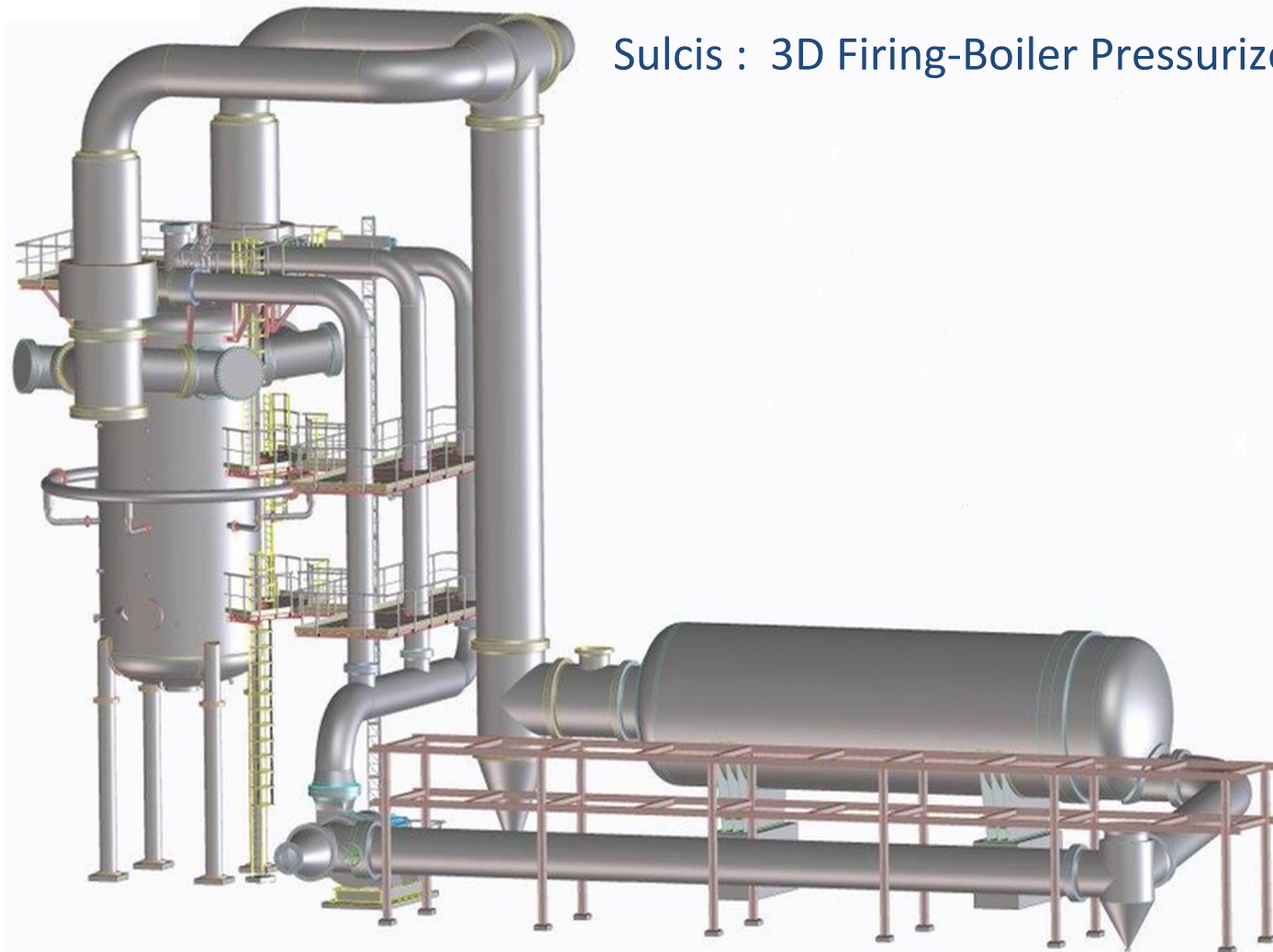
Model numerical parameters adjustments and validation, 5 to 50 MWt

on the more promising set up

to cross off any process risk in the pathway to demo and industrial units

## FPOC: Combustor Scale-Up

Sulcis : 3D Firing-Boiler Pressurized Loop 50+ MWt





THANK YOU FOR YOUR ATTENTION